Electrochemical Engineering
Electrochemical Engineering

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WILEY
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Preface

Given the existing books on electrochemistry and electrochemical engineering, what do we hope to accomplish with this text? The answer is twofold. First, it is our goal to provide enough of the fundamentals to enable students to approach interesting problems, but not so much that new students are overwhelmed. In doing this, we have attempted to write with the student in mind, and choices regarding content, examples, and applications have been made with the aim of helping students understand and experience the important and exciting discipline of electrochemical engineering. The text has a large number of worked out examples, includes homework problems for each chapter, and uses consistent nomenclature throughout in order to facilitate student learning. Our second objective is to integrate key applications of electrochemical engineering with the relevant fundamentals in a single book. We have found applications to be of great interest to students. Importantly, applications provide students with the opportunity to practice in a meaningful way the fundamentals that they have learned. We have made a deliberate effort to tie the investigation of the applications directly back to the fundamental principles.

The book is intended for senior-level engineering students and entering graduate students in engineering and the sciences. No knowledge of electrochemistry is assumed, but an undergraduate training in thermodynamics, transport, and freshman chemistry is needed. A basic knowledge of differential equations is also recommended. Historically, electrochemical engineering is closely associated with chemical engineering and chemistry. However, the lines between disciplines are becoming increasingly blurred, and today we find mechanical engineers, material science engineers, and physicists engaged in electrochemical engineering. We have attempted to broaden our view of electrochemical engineering both to appeal to a larger audience and to expand the exposure of students to new areas and opportunities.

The text is divided into two parts. The first six chapters cover essential topics in a familiar order: an introduction, thermodynamics, kinetics, and mass transport. Also included in these fundamentals is a chapter on electrode structures and one on electroanalytical techniques. The remaining chapters cover applications of electrochemical engineering. It is assumed that the student will have mastered the fundamental chapters before starting on the applications. The application-focused chapters comprise batteries, fuel cells, double-layer capacitors, energy storage systems for vehicles, electrodeposition, industrial electrolysis, semiconductor electrodes, and corrosion. For the most part, the instructor can pick and choose which application chapters to cover; and these applications can be presented in any order. Although not exhaustive, the applications selected represent important applications of electrochemical engineering.

Each chapter begins with a short biography of one of the founders in electrochemistry and electrochemical engineering from the twentieth century. Even though not essential to the technical material presented, writing these short sketches was often personal and deeply satisfying. In general, our focus was on the accomplishments and impact of these remarkable individuals. The selection of whom to profile was also personal and, without question, subjective. Other than space limitations, there can be no justification for omitting pioneers such as Alan Bard and Norbert Ibl.

The authors have used this material to teach introductory electrochemical engineering courses at Georgia Institute of Technology and Brigham Young University. Many of the chapters were drastically revised after the first teaching. Again, our objective was to create a textbook suitable for classroom teaching. Many of the problems presented at the end of the chapters have been honed through homework assignments and on examinations. In fact, these problems and our lectures guided what content to include in the text—we sought to eliminate from the book content not
addressed in class or not suitable for practice in the form of problems. Our experience has been that in a one semester course only a couple of the application chapters can be completed in addition to the first six fundamental chapters. We have purposely included references only sparingly in the text itself. While important references for each topic are found at the end of each chapter, we made no attempt to meticulously ascribe credit—our thinking was a highly annotated text is not important to beginning students and actually presents an additional barrier to learning.

The journey of writing this book has been immensely rewarding and not surprisingly a bit longer than anticipated. We have so many colleagues, students, friends, and family members to thank. Their support and encouragement was beyond heartening.

2017

Thomas F. Fuller
John N. Harb
List of Symbols

$a$ specific interfacial area, m$^{-1}$
$a_i$ activity of species $i$, unitless
$A$ area, m$^2$
$A_c$ cell or electrode area, m$^2$
$A_r$ Archimedes number, unitless
$b$ Tafel slope, V per decade
$B$ Debye constant for solvent, (kg/mol)$^{1/2}$ m$^{-1}$
$c$ speed of light, $2.99792 \times 10^8$ m s$^{-1}$
$c_i$ concentration of species $i$, mol m$^{-3}$
$C$ capacitance, F
$C_d$ differential capacitance, F
$C_{DL}$ double layer capacitance per unit area, F m$^{-2}$
$C_p$ battery capacity offset, unitless
$d$ distance, m
$d_h$ hydraulic diameter, m
$D_i$ molecular diffusivity of species $i$, m$^2$ s$^{-1}$
$E$ elastic modulus, Pa
$E_a$ activation energy, J/mol
$E_g$ energy gap, eV
$f$ frequency, Hz
$f_i$ fugacity of species $i$, Pa
$F$ Faraday’s constant, 96485 C per equivalent
$F_s$ component of force, N
$g$ acceleration of gravity, m s$^{-2}$
$G$ Gibbs energy, J mol$^{-1}$
$G$ conductance, $\Omega^{-1}$
$Gr$ Grashof number, unitless
$h$ thickness, gap in electrolysis cells, m
$h$ Planck’s constant, J-s
$H$ Enthalpy, J mol$^{-1}$
$i, i$ current density, A m$^{-2}$
$I$ current, A
$i_o$ exchange current density, A m$^{-2}$
$I_p$ photon flux, s$^{-1}$ m$^{-2}$
$J_i$ molar flux of species $i$, mol m$^{-2}$ s$^{-1}$
$k_a, k_c$ anodic and cathodic reaction rate constants
$k_c$ mass transfer coefficient, m s$^{-1}$
$k$ thermal conductivity, W m$^{-1}$ K$^{-1}$
$K$ equilibrium constant, unitless
$L$ characteristic length, m
$L_p$ diffusion length, m
$m$ mass, kg
$m$ molality, mol kg$^{-1}$
$m$ mass flow, kg s$^{-1}$
$M_i$ molecular weight, g mol$^{-1}$ or kg mol$^{-1}$
$n$ number of electrons transferred
$n$ number density of electrons, m$^{-3}$
$n_i$ number of moles of species $i$, mol
$n_i$ number density of electrons in intrinsic semiconductor, m$^{-3}$
$N_{AV}$ Avogadro’s number
$N_A$ number density of acceptor atoms, m$^{-3}$
$N_D$ number density of donor atoms, m$^{-3}$
$N_i$ molar flux of species $i$ relative to stationary coordinates, mol m$^{-2}$ s$^{-1}$
$p$ pressure, Pa
$p$ number density of holes, m$^{-3}$
$P$ power, W
### List of Symbols

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<thead>
<tr>
<th>Symbol</th>
<th>Description</th>
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<tbody>
<tr>
<td>P</td>
<td>perimeter, m</td>
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<tr>
<td>q</td>
<td>fundamental charge, $1.602 \times 10^{-19}$ C</td>
</tr>
<tr>
<td>$q'$</td>
<td>charge per unit surface area, C m$^{-2}$</td>
</tr>
<tr>
<td>$\dot{q}$</td>
<td>rate of heat generation, W</td>
</tr>
<tr>
<td>Q</td>
<td>charge, C or A h</td>
</tr>
<tr>
<td>r</td>
<td>radius, m</td>
</tr>
<tr>
<td>R</td>
<td>universal gas constant, 8.314 J mol$^{-1}$ K$^{-1}$</td>
</tr>
<tr>
<td>$R_\Omega$</td>
<td>ohmic resistance, $\Omega$ or $\Omega$ m$^2$</td>
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<tr>
<td>Re</td>
<td>Reynolds number, unitless</td>
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<tr>
<td>$R_\text{v}$</td>
<td>homogeneous reaction rate, mol m$^{-3}$ s$^{-1}$</td>
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<td>$s_i$</td>
<td>stoichiometric coefficient, unitless</td>
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<td>S</td>
<td>electrical conductance, S</td>
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<td>S</td>
<td>entropy, J mol$^{-1}$ K$^{-1}$</td>
</tr>
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<td>Sh</td>
<td>Sherwood number, unitless</td>
</tr>
<tr>
<td>Sc</td>
<td>Schmidt number, unitless</td>
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<tr>
<td>t</td>
<td>time, s</td>
</tr>
<tr>
<td>$t_i$</td>
<td>transference number of species $i$, unitless</td>
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<tr>
<td>$T$</td>
<td>temperature, K, or °C</td>
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<tr>
<td>U</td>
<td>equilibrium potential, V</td>
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<tr>
<td>$u_i$</td>
<td>mobility of ion, m$^2$ mol J$^{-1}$ s$^{-1}$</td>
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<tr>
<td>v</td>
<td>velocity, m s$^{-1}$</td>
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<td>V</td>
<td>electric potential or voltage, V</td>
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<tr>
<td>$v_s$</td>
<td>superficial velocity, m s$^{-1}$</td>
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<tr>
<td>$\tilde{v}$</td>
<td>volumetric flowrate m$^3$ s$^{-1}$</td>
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<td>$\gamma$</td>
<td>volume, m$^3$</td>
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<td>W</td>
<td>work, J</td>
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<td>$W$</td>
<td>width of depletion layer, m</td>
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<td>$w$</td>
<td>molar flowrate, mol s$^{-1}$</td>
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<td>Wa</td>
<td>Wagner number, unitless</td>
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<td>$x_i$</td>
<td>mole fraction of species $i$ in condensed phase, unitless</td>
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<td>$y_i$</td>
<td>mole fraction of species $i$ in gas phase, unitless</td>
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<td>$z_i$</td>
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<td>$\varepsilon$</td>
<td>porosity, unitless</td>
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<td>$\varepsilon_o$</td>
<td>permittivity of free space, $8.854 \times 10^{-12}$ C V$^{-1}$ m$^{-1}$</td>
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<td>$\varepsilon_r$</td>
<td>relative permittivity, unitless</td>
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<td>strain, unitless</td>
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<td>$\eta$</td>
<td>current efficiency</td>
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<td>$\eta_{coul}$</td>
<td>coulombic efficiency, unitless</td>
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<td>$\eta_f$</td>
<td>faradaic efficiency, unitless</td>
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<td>$\eta_S$</td>
<td>surface overpotential, V</td>
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<td>$\kappa$</td>
<td>electrical conductivity, S m$^{-1}$</td>
</tr>
<tr>
<td>$\lambda$</td>
<td>Debye length, or wavelength, m</td>
</tr>
<tr>
<td>$\lambda_i$</td>
<td>absolute activity</td>
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<td>$\lambda_i$</td>
<td>equivalent conductance, S m$^{-2}$ equivalent$^{-1}$</td>
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<tr>
<td>$\Lambda$</td>
<td>conductance, S m$^{-1}$</td>
</tr>
<tr>
<td>$\mu$</td>
<td>viscosity, Pa s</td>
</tr>
<tr>
<td>$\mu_i$</td>
<td>chemical potential, J mol$^{-1}$</td>
</tr>
<tr>
<td>$\nu$</td>
<td>kinematic viscosity, m$^2$ s$^{-1}$</td>
</tr>
<tr>
<td>$\nu$</td>
<td>scan rate, V s$^{-1}$</td>
</tr>
<tr>
<td>$\nu_i$</td>
<td>stoichiometric coefficient, unitless</td>
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<tr>
<td>$\xi$</td>
<td>electro-osmotic drag coefficient, unitless</td>
</tr>
<tr>
<td>$\rho$</td>
<td>mass density, kg m$^{-3}$</td>
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<td>$\rho_e$</td>
<td>charge density, C m$^{-3}$</td>
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<td>$\sigma$</td>
<td>electrical conductivity of solid, S m$^{-1}$; or surface energy, J m$^{-2}$</td>
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<td>characteristic time, s</td>
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<tr>
<td>$\tau$</td>
<td>tortuosity, dimensionless</td>
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<td>$\phi$</td>
<td>potential, V</td>
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<td>$\Phi$</td>
<td>quantum yield</td>
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<td>$\varphi$</td>
<td>gas holdup, osmotic coefficient, unitless</td>
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<td>$\omega$</td>
<td>angular frequency, rad s$^{-1}$</td>
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### Subscripts and Superscripts

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<td>avg</td>
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<td>bubble</td>
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<tr>
<td>c</td>
<td>charge, cathode, or cutoff frequency</td>
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<tr>
<td>cb</td>
<td>conduction band</td>
</tr>
<tr>
<td>ct</td>
<td>charge transfer</td>
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<td>d</td>
<td>discharge</td>
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<tr>
<td>e</td>
<td>electrolyte</td>
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<td>eff</td>
<td>effective quantity</td>
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<td>f</td>
<td>formation</td>
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<tr>
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<td>metal</td>
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<td>$o$</td>
<td>value at standard or reference conditions</td>
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<td>open circuit voltage</td>
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<td>photon</td>
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<td>reaction</td>
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<td>$s$</td>
<td>solution, separator, or surface</td>
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<td>space charge</td>
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<td>$vb$</td>
<td>valence band</td>
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<td>$\infty$</td>
<td>bulk value far from electrode</td>
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<tr>
<td>$o$</td>
<td>initial value</td>
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<td>$\theta$</td>
<td>equilibrium potential at reference conditions</td>
</tr>
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<td>$*$</td>
<td>ideal gas</td>
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</table>
About the Companion Website

This book is accompanied by a companion website:

www.wiley.com/go/fuller/electrochemicalengineering

The website features:

- Powerpoint slides for figures from the text
- Complete solution manual to end of chapter problems
- Excel files for data sets used in student problems and chapter illustrations
Charles W. Tobias was born on November 2, 1920 in Budapest, Hungary and died in 1996 in Orinda, California. He describes his family as an “engineering family” and realized that he would be an engineer from the age of 4 or 5. Music was a lifelong passion, but engineering was his career. Tobias was inspired to select chemical engineering by his high school chemistry teacher. He attended the University of Technical Sciences in Budapest, where he obtained his Ph.D. in 1946. He was part of the Hungarian diaspora, fleeing Hungary in 1947 as the Communists were taking over the government. He traveled to Berkeley to pursue postdoctoral studies at the University of California where his brother was already working for Ernest O. Lawrence at the University’s radiation laboratory. W.M. Latimer, a pioneer in the thermodynamics of electrolytes and Tobias’s new boss, directed him to “... build up engineering electrochemistry here, and it should be the best in the world.” By all measures, he succeeded. He began as an instructor in the newly formed Department of Chemical Engineering and then became an Assistant Professor in 1950 and Professor in 1960. He also chaired the department from 1967 until 1972.

Charles Tobias is considered by many to be the father of modern electrochemical engineering. He added discipline and rigor, putting many of the principles on a sound theoretical footing. He studied fluid flow, electric potential fields, thermodynamic and materials properties, and mass transfer, linking his findings into a new discipline. Tobias was instrumental in moving the field from largely empirical approaches to a quantitative science that addressed scale-up and optimization. Professor Tobias is also credited with founding the electrochemical research program at Lawrence Berkeley National Laboratory, which for decades was the most influential electrochemistry group. He is reported to have started the first “electrochemical engineering” course. Professor Tobias joined with Paul Delahay in 1961 to edit a new monograph series entitled Advances in Electrochemistry and Electrochemical Engineering.

Professor Tobias had a long and productive involvement in the Electrochemical Society. He won several awards, including the Society’s highest honor, the Acheson award. He served as President of the Electrochemical Society from 1970 to 1971 as well as an editor for the Journal of the Electrochemical Society for many years. As a result, he had a large influence on the structure and operation of the Society. Tobias brought the same philosophy of increasing the scientific rigor and quantitative engineering to the Society. He was also President of the International Society of Electrochemistry (1977–1978). In 2003, the Tobias Award of the Electrochemical Society was established to recognize outstanding scientific and/or engineering work in fundamental or applied electrochemistry by a young investigator.

Although Tobias had an immeasurable impact on the field of electrochemical engineering and was elected a member of the National Academy of Engineering, he was not particularly aggressive in publishing. One of his most significant findings was the use of propylene and ethylene carbonates for lithium batteries, but it was never published beyond a laboratory report. Nonetheless, Dr. Tobias believed that knowledge should always be shared—only ignorance needs secrecy. Much of the information here was derived from the chemical heritage foundation’s oral history, which delivers an excellent portrait of his life.


Image Source: Courtesy of UC Berkeley College of Chemistry.
Chapter 1

Introduction and Basic Principles

Welcome to this introductory text about electrochemical engineering. If you are like most people, you probably have little idea of what “electrochemical engineering” is and why it is important. That’s okay. This book is to help you answer those questions and to prepare you to work in this exciting area. Electrochemistry is a branch of chemistry that studies the chemical changes that occur due to the flow of electrical current or, conversely, the production of electricity from chemical changes. As engineers, we are interested in the application of scientific knowledge, mathematical principles, and economic analyses to the design, manufacture, and maintenance of products that benefit society. It’s not surprising, then, that electrochemical engineering has strong historical ties to the profession of chemical engineering.

Almost invariably, application of the principles of electrochemistry to develop products or devices requires consideration of an electrochemical system. An engineering system consists of multiple components that work together in a concerted manner. In addition to electrochemistry, other topics such as heat transfer, structural analysis, and materials science are critical to the design and operation of electrochemical systems. Today, we find engineers and scientists of all disciplines engaged in electrochemistry and collaborating in the design of electrochemical systems.

As with any topic, electrochemical engineering includes a new set of terminology that must be learned. There are also several conventions of practical importance. Hence, this chapter will introduce you to the key vocabulary of the discipline, as well as to some of the central aspects of electrochemical systems. In order to do this, we begin by looking at an electrochemical cell.

1.1 ELECTROCHEMICAL CELLS

Electrochemical cells, such as the cell illustrated in Figure 1.1, lie at the heart of electrochemical systems. A typical electrochemical cell consists of two electrodes: an anode where oxidation occurs and a cathode where reduction takes place. Electrons move through an external circuit via an electronic conductor that connects the anode and cathode. The liquid solution that is between the two electrodes is the electrolyte. The electrolyte does not conduct electrons and does not contain any free electrons. It does, however, contain a mixture of negatively charged ions (anions) and positively charged ions (cations). These ions are free to move, which allows them to carry current in the electrolyte.

The reactions take place at the electrode surface and are called heterogeneous electron-transfer reactions. For example, the electrodeposition of copper in the cell shown in Figure 1.1 can be written as

\[ \text{Cu}^{2+}_{(aq)} + 2e^- \rightarrow \text{Cu}_{(s)} \]  

(1.1)

Copper ions in solution accept two electrons from the metal and form solid copper. The reaction is described as heterogeneous because it takes place at the electrode surface rather than in the bulk solution; remember, there are no free electrons in the solution. Importantly, then, we see that electrochemical reactions are surface reactions. The metal that accepts or supplies electrons is the electrode. As written, copper ions gain electrons and therefore are reduced to form copper metal. When reduction occurs, the electrode is called the cathode.

In the same cell, the reaction that takes place on the other electrode is

\[ \text{Zn}_{(s)} \rightarrow \text{Zn}^{2+}_{(aq)} + 2e^- \]  

(1.2)

The zinc metal is oxidized, giving up two electrons and forming zinc ions in solution. When oxidation occurs at the surface, the electrode is called the anode.

Both the copper and zinc reactions written above (Equations 1.1 and 1.2) are half-cell reactions, meaning that they describe a reaction that takes place at one of the electrodes. Half-cell reactions always have electrons as either a reactant or a product. Also, charge is always balanced in half-cell reactions. Charge balance means...
that the net charge on one side of the equation must equal the net charge on the other side of the equation. For example, in the above equation, the net charge on the Zn (left side of the equation) is zero. This value is equal to the net charge for the other side, which is \((+2) + 2(-1) = 0\). Charge balance is no surprise since electrochemical reactions simply add or remove electrons.

The cell illustrated in Figure 1.1 is called a Daniell cell and is named after John Frederic Daniell, who invented the cell in 1836. In this cell, the electrodes themselves (solid Zn and Cu) participate in the electrochemical reactions as either a reactant or a product. This is not always the case, as we shall see later. The electrons for the reduction of Cu\(^{2+}\) come from the other electrode where the oxidation of Zn takes place. The electrons that are liberated from zinc oxidation at the anode travel through an external circuit to participate in the reduction reaction at the cathode. The movement of electrons corresponds to an electrical current flowing through the external circuit. The anode and cathode reactions can be combined to give an overall cell reaction, also called the \textit{full-cell reaction}. Note that there are no electrons in the overall reaction, but charge is still balanced.

\[
\text{Zn(s)} + \text{Cu}^{2+} \text{aq} \rightarrow \text{Zn}^{2+} \text{aq} + \text{Cu(s)} \quad (1.3)
\]

In other words, the exact number of electrons released from oxidation is used for reduction. Similarly, for each copper ion that is reduced, one zinc ion is formed. Because there is a production of charge at the anode and a consumption of charge at the cathode, there is a net movement of charge in solution from the anode to the cathode. Thus, there is also a current flowing in the solution, but the net charge in the solution is unchanged.

The flow of current in an electrochemical cell is shown in Figure 1.1. Note that, by definition, current in the external circuit is opposite (cathode to anode) to the direction that electrons flow. As illustrated in the figure, current flows counterclockwise in a continuous circuit that includes the solution and the external circuit. The electrochemical reactions are the means by which current flows from the electrode to the solution (anode) and from the solution to the electrode (cathode) as part of this circuit. These reactions will not take place if the circuit is broken. This circuit is most commonly “broken” by disconnecting the external connection between the electrodes. In the absence of this external connection, the cell is at \textit{open circuit}, and there is no net reaction at either electrode. Finally, we note that the name “electrochemical” refers to the fact that the \textit{chemical} changes are connected to the flow of \textit{electric} current. Some of the additional aspects of electrochemical reactions are discussed in the next section.

### 1.2 CHARACTERISTICS OF ELECTROCHEMICAL REACTIONS

Electrochemical reactions are reactions where electrons are transferred through a conductor from the species being oxidized to that being reduced. Most of the unique and important properties of electrochemical reactions are the result of the way that these electrons are transferred. These characteristics include the following:

\textit{Separation of the oxidation (anodic) and reduction (cathodic) reactions}. Because electrons are transferred through a conductor, the oxidation and reduction can
take place on two different electrodes. This situation is the most common type of configuration for an electrochemical cell, as already illustrated.

**Use of electrons to perform work.** In cells like the Daniell cell introduced in Section 1.1, electrons move spontaneously from the anode to the cathode when the circuit is closed (completed), because the energy of electrons in the anode is higher than the energy of electrons in the cathode. Some of that extra electron energy can be used to perform work by passing the electrons (current) through a load (e.g., an electronic device). Perhaps the most familiar application of this concept is in the battery that you use to power your phone or computer, where you are using electron energy to send messages to your friends or to complete your homework.

**Direct measurement of reaction rates.** Typically, it is difficult to measure directly the rates of chemical reactions. However, since electron transfer in electrochemical reactions takes place through a conductor, the reaction rate is easy to measure—you just measure the electric current passing in the wire between the electrodes. That current is directly related to the reaction rate at each of the two electrodes. We will explore this later in the chapter when we discuss Faraday’s law.

**Control of the direction and rate of reaction.** Because electrons participate in both the oxidation and reduction reactions as either a product or a reactant, we can change the rate of reaction by changing the difference in potential between the electrodes. The electric potential is a measure of the electron energy. By adjusting the potential, we can speed up the reactions, slow them down, or even make them go in the reverse direction.

This textbook will help you to understand and to use the powerful properties of electrochemical reactions to design useful products. In the application chapters of the book, you will have the opportunity to see what others have done with electrochemical systems to create devices and processes that benefit humankind. In preparation, the next section of this chapter provides a brief overview of the applications that will be considered in order to illustrate the importance of electrochemical systems. However, before doing that, let’s consider some additional aspects of electrochemical reactions.

In the Zn/Cu cell considered previously, the electrodes participated directly as either a reactant (Zn) or a product (Cu). In many instances, the electrodes do not participate beyond supplying or removing electrons. In these instances, the electrodes are called **inert**. Each of the electrochemical reactions considered in the Daniell cell involved one solid species and one aqueous species. This is by no means a requirement or even typical. Reactants and products in electrochemical reactions can be solids, liquids, dissolved species, or gases. The evolution of hydrogen gas, for instance,

\[
2\text{H}^+ + 2\text{e}^- \rightarrow \text{H}_2(g) \tag{1.4}
\]

is a reduction (cathodic) reaction that occurs at an inert electrode. Here, the reactant is dissolved in solution and the product is a gas. The oxidation of iron(II) to iron(III) provides another example:

\[
\text{Fe}^{2+}_{(aq)} \rightarrow \text{Fe}^{3+}_{(aq)} + \text{e}^- \tag{1.5}
\]

In this case, both the reactant and product are dissolved species.

In looking at the reactions for the Daniell cell, we note that copper ions gained two electrons, zinc lost two electrons to form zinc ions, hydrogen ions gained one electron each to produce hydrogen gas, and a ferrous ion lost an electron to form a ferric ion. You may be wondering how we know how many electrons will be transferred and the direction in which the reaction will go. The direction depends on potential as we will see in the next two chapters. However, the oxidation and reduction products are determined by the electronic structure of the participating species. You undoubtedly learned about oxidation states in your beginning chemistry class, and those same principles apply here. Let’s consider a couple of simple examples just to illustrate the concept. Sodium is an alkali metal and has a single electron in its outer electron shell. Whenever possible, sodium tends to give up that electron, leaving it with a +1 charge and a full outer shell. Thus, the stable state for a sodium ion is Na⁺. Similar logic can be used for the other alkali metals. In the second column of the Periodic Table you have alkaline-earth metals, such as magnesium or calcium. These elements have two electrons in their outer shell and, therefore, yield ions with a +2 charge such as Mg²⁺ or Ca²⁺, using rationale similar to that used for the alkali metals. Moving to the other side of the Periodic Table, we find chlorine that has seven electrons in its outer shell. Chlorine likes to pick up an extra electron in order to complete that shell. Therefore, it forms Cl⁻. Finally, the electronic structure of some elements (e.g., most transition metals) allows them to form ions with different oxidation states; for example, iron can form Fe²⁺ or Fe³⁺.

Fortunately, you don’t need to memorize the Periodic Table or to look up the electronic structure of an element every time to determine the relevant oxidation state or half-cell reaction. Tables of known electrochemical reactions are available, and a short list appears in Appendix A of this book. These tables not only show the reactions, but also give the standard potential for each reaction. This standard potential is extremely important as we will see in the next chapter. Note that, by convention, the reactions in Appendix A are written as reduction reactions, but we can treat them as being reversible.
ILLUSTRATION 1.1

Use the table in Appendix A to find the two half-cell reactions and combine them to determine the full-cell reaction.

a. **Corrosion of iron in an oxygen-saturated acid solution.** On one electrode, iron metal is oxidized to form $\text{Fe}^{2+}$; on the other electrode, oxygen is reduced. Entry 18 shows the reduction of iron:

$$\text{Fe}^{2+} + 2e^- \rightarrow \text{Fe} - 0.440 \text{ V}$$

We reverse the direction to get the oxidation of iron:

$$\text{Fe} \rightarrow \text{Fe}^{2+} + 2e^-$$

The reduction of oxygen in acid is given by entry 4:

$$\text{O}_2 + 4\text{H}^+ + 4e^- \rightarrow 2\text{H}_2\text{O}$$

These two reactions are then combined. The iron oxidation reaction is first multiplied by two so that the electrons cancel out when the equations are added together:

$$\text{O}_2 + 4\text{H}^+ + 2\text{Fe} \rightarrow 2\text{H}_2\text{O} + 2\text{Fe}^{2+}$$

b. **Deposition of silver from an alkaline solution.**

$$\text{Ag}^+ + e^- \rightarrow \text{Ag} \quad \text{entry 6}$$

$$4\text{OH}^- \rightarrow \text{O}_2 + 2\text{H}_2\text{O} + 4e^- \quad \text{entry 9}$$

The silver reduction reaction is multiplied by four and added to the oxidation reaction to provide the full-cell reaction:

$$4\text{Ag}^+ + 4\text{OH}^- \rightarrow \text{O}_2 + 2\text{H}_2\text{O} + 4\text{Ag}$$

1.3 IMPORTANCE OF ELECTROCHEMICAL SYSTEMS

Electrochemical systems are not only essential for our society but are also common in everyday life. Imagine a world without batteries to power your personal electronic devices. How would travel change without low-cost aluminum that is essential for aircraft? What if corrosion of the steel in bridges, the hulls of ships, superstructures of buildings, and pipelines couldn’t be controlled? These examples, electrochemical energy storage, industrial electrolysis, and corrosion, are some of the major applications of electrochemical engineering. Following development of the fundamental principles of electrochemical engineering, these and other applications are covered in separate chapters.

We all know that the storage of energy using batteries (Chapters 7 and 8) is an essential feature for countless technologies. The size of the global battery market is more than 50 billion dollars annually. Applications of batteries are widespread in society, ranging from basic consumer electronics, to automobiles, implanted medical devices, and space travel. Energy storage is needed where portability is required, emergency power is desired, or simply when electrical demand and supply are not matched. Batteries store energy chemically and convert that energy to electricity as needed. For many applications, the conversion between chemical and electrical energy must be extremely efficient and, in some cases, nearly reversible in order for batteries to be practical. Electrochemical double-layer capacitors (Chapter 11) can also be used to store energy.

The purpose of industrial electrolysis is to use electrical energy to convert raw materials into desired products. This transformation of raw materials takes place in an electrochemical reactor. Industrial electrolytic processes (Chapter 14) consume about 6% of the U.S. electricity supply. Although a number of metals and other materials can be produced electrochemically, the main products of electrolysis are aluminum, chlorine, and sodium hydroxide (caustic soda). Low-cost electricity and electrochemical routes for production transformed aluminum from an expensive and rarely used metal to a commodity material that is essential for society. Chlorine and sodium hydroxide, produced simultaneously on a huge scale by electrolysis, are required for the production of a variety of materials, including plastics, paper, soaps, solvents, and a large number of other chemicals.

The many desirable properties of metals have led to their widespread use in industry and, frankly, in nearly every aspect of our lives. Corrosion (Chapter 16) is the unwanted attack of metals by their environment. The manufacture of metals is sometimes done electrochemically as described above for the production of aluminum. We can think of corrosion as the reverse process, by which metals are converted back into their oxide form. This cycle is illustrated in Figure 1.2. The process of corrosion is electrochemical in nature. The global economic cost of corrosion has been estimated to be several trillion dollars annually. Therefore, it is important that engineers understand the conditions under which corrosion is likely to occur. They should also be able to measure, predict, and mitigate the negative impacts of corrosion. Avoidance of corrosion is incorporated into the appliances found in our homes. Additionally, corrosion prevention is essential for maintaining the integrity of the bridges over which we travel, and an integral part of the design of natural gas and oil pipelines that supply our energy. These are just a few of the areas where understanding corrosion is important.

Electrodeposition is the electrochemical deposition of a metal onto a surface (Chapter 13). Electrodeposition is
fundamental principles provide the foundation for all of the applications mentioned above. We begin by introducing some basic terminology, as well as reviewing scientific units and the conventions adopted in this text.

### 1.4 SCIENTIFIC UNITS, CONSTANTS, CONVENTIONS

There are seven base units within the International System of Units (SI system), as shown in Table 1.1 for quick reference. Except for luminous intensity, all of the quantities are used extensively in this text. Among the base units is electric current, $I$, which is critical for the examination of electrochemical systems. Electric current is measured in amperes [A].

Table 1.2 presents derived units that are used widely in this text and are associated with electrochemical engineering. For each quantity, the name and the SI symbol for the quantity is presented. Our general practice will be to place units in brackets, for example, [Pa·s]. When working problems, dimensional consistency is critical; it will also help you to avoid calculation errors. Therefore, for convenience, the table provides the dimensions of these derived quantities written in terms of both the base units and in an alternative form convenient for calculations. For instance, the units for capacitance \([m^2 \cdot kg^{-1} \cdot s^4 \cdot A^2]\) can be written more compactly in terms of other derived units \([C \cdot V^{-1}]\), which will usually be more intuitive and easier to remember when checking for dimensional consistency. Finally, the last column provides the variable symbol used in this text to represent the physical quantity. Where possible, we have used the most common nomenclature to represent these quantities. A detailed list of the nomenclature is provided at the beginning of the book. It is important to note that sometimes the nomenclature for a variable may be the same as the unit. To minimize confusion, remember that variables and fundamental physical constants are in *italics*, whereas the units will not be italicized. Thus, $V$

<table>
<thead>
<tr>
<th>Quantity</th>
<th>Name of unit</th>
<th>Symbol for unit</th>
<th>Nomenclature used in text</th>
</tr>
</thead>
<tbody>
<tr>
<td>Length</td>
<td>meter</td>
<td>[m]</td>
<td>$L$</td>
</tr>
<tr>
<td>Mass</td>
<td>kilogram</td>
<td>[kg]</td>
<td>$m$</td>
</tr>
<tr>
<td>Mole</td>
<td>mole</td>
<td>[mol]</td>
<td>$n_i$</td>
</tr>
<tr>
<td>Time</td>
<td>second</td>
<td>[s]</td>
<td>$t$</td>
</tr>
<tr>
<td>Temperature</td>
<td>kelvin</td>
<td>[K]</td>
<td>$T$</td>
</tr>
<tr>
<td>Current</td>
<td>ampere</td>
<td>[A]</td>
<td>$I$</td>
</tr>
<tr>
<td>Luminous intensity</td>
<td>candela</td>
<td>[cd]</td>
<td>–</td>
</tr>
</tbody>
</table>
represents the potential of an electrochemical cell, whose units are volts [V]. Similarly, A is area [m²], whereas [A] is the unit for current in amperes. Most often we will be dealing with scalar quantities. However, occasionally we will encounter vector quantities, ones that have both magnitude and direction. These quantities will be written in bold face. For example, velocity, a vector quantity, is written with the symbol \( \mathbf{v} \).

The coulomb [C] is an SI-derived unit of electrical charge—simply the amount of charge that passes with a current of 1 ampere for 1 second. The elementary charge, denoted with \( q \), is a fundamental physical constant. The value of \( q \) is \( 1.602177 \times 10^{-19} \text{C} \) and equal to the charge of a single proton. Additional essential fundamental constants are provided in Appendix B.

### 1.5 Faraday’s Law

In this section, we examine Faraday’s law, which is the relationship between the amount of current that flows through the external circuit and the amount of material that is either consumed or produced in a half-cell reaction. To explore how this works, let’s return once again to the zinc reaction:

\[
\text{Zn(s)} \rightarrow \text{Zn}^{2+} + 2e^- \tag{1.6}
\]

From the half-cell equation, it is apparent that two electrons are produced for every zinc atom that reacts. Typically, it is more convenient to work in terms of moles rather than atoms. Therefore, two moles of electrons are produced for every mole of zinc atoms that is oxidized. As you can see, we can easily relate the moles of electrons to the moles reacted or produced for any species in a given half-cell reaction.

The next step is to relate the moles of electrons to the current that we measure through the external circuit. To do this, it is customary to introduce a new unit of charge—an equivalent. An equivalent is defined as a mole of charge (either positive charge or negative charge, it does not matter). The number of equivalents of a compound is simply the amount of the substance (in moles) multiplied by the absolute value of its charge, \( z_e \). For instance, one mole of Na⁺ is 1 equivalent, whereas one mole of Ca²⁺ would be 2 equivalents. Because the sign of the charge does not matter, one mole of electrons is equal to 1 equivalent of charge.

The external current is expressed in amperes [A] or C·s⁻¹. Therefore, we need a relationship between coulombs [C] and equivalents. That relationship is called Faraday’s constant, \( F \), which has a value of 96,485 C/equivalent. Faraday’s constant can also be expressed in terms of two other constants: the fundamental unit of charge, \( q \), and Avogadro’s number, \( N_{AV} \).

\[
F = qN_{AV}. \tag{1.7}
\]

This expression is another way of stating that an equivalent is a mole of charge, since \( q \) is the amount of charge on a proton in coulombs. We also need a relationship between the current, \( I \) [A], and the total charge passed in coulombs. That relationship is

\[
Q = \int I dt, \tag{1.8}
\]

where \( Q \) is the charge in [C], \( I \) in [A], and \( t \) in [s]. In situations where the current is constant, Equation 1.8 simplifies to

\[
Q = It. \tag{1.9}
\]

We now have the pieces that we need to write the relationship between the current in the external circuit and the
amount of a substance that is either reacted or produced. Let’s apply what we have learned to the zinc electrode.

**ILLUSTRATION 1.2**

For the oxidation of zinc, a current of 12 A passes for 2 hours. How much zinc reacts? Provide the answer in terms of mass and the moles of zinc. The reaction is

\[
\text{Zn(s)} \rightarrow \text{Zn}^{2+} + 2e^-
\]

First, the total charge passed is determined from Equation 1.9.

\[
Q = It = \frac{12[\text{C}]}{[\text{s}]} \times \frac{2[\text{h}]}{[\text{h}]} \times 3600[\text{s}] = 86,400[\text{C}] 
\]

The number of moles of zinc is proportional to the charge passed. From the stoichiometry of the oxidation reaction, for each mole of zinc two moles of electrons are released. Thus,

\[
m_{\text{Zn}} = n_{\text{Zn}} = \frac{Q}{2F} = \frac{(86400[\text{C}])}{(2[\text{equiv/mol}]) (96485 \text{[C/equiv]})} = 0.448 \text{ mol Zn}
\]

The mass of zinc consumed is simply the moles times the molecular weight:

\[
m_{\text{Zn}} = M_{\text{Zn}}n_{\text{Zn}} = (65.38)(0.448) = 29.3 \text{ g Zn}.
\]

Let’s now generalize what we have done to this point. Any half-cell reaction can be expressed in the following form:

\[
\sum_i s_i A_i = ne^- 
\]

where \(s_i\) is the stoichiometric coefficient for species \(i\), which can be either positive or negative, \(A_i\) is the symbol for the specific species (e.g., \(\text{Zn}^{2+}\)), and \(n\) is the number of electrons involved in the reaction. The mass of species \(i\) that is either consumed or produced is equal to

\[
m_i = \frac{M_i Q}{n_i F} = \frac{M_i \left[\frac{\text{g}}{\text{mol}}\right]}{n_i \left[\frac{\text{equiv}}{\text{mol}}\right]} \frac{Q [\text{C}]}{F \left[\frac{\text{C}}{\text{equiv}}\right]}, \quad (1.11a)
\]

where \(M_i\) is the molecular weight of species \(i\). This equation is known as Faraday’s law. We have been careful to include the stoichiometric coefficient with Equation 1.11a. However, most often Faraday’s law is written as

\[
m_i = \frac{M_i Q}{n F}. \quad (1.11b)
\]

We will also use this form. When using Equation 1.11b, you need to recognize that \(n\) represents the number of electrons per species \(i\). Look carefully at the examples that follow.

Although Equation 1.11 is useful, the most important aspect of this section is the process that we used to develop the equation. We started with charge, \(Q\), in standard units of [C]. This charge is directly related to the current that we measure in [A] as a function of time. We then converted that charge to moles of electrons (equivalents). The moles of electrons were then related through the half-cell reaction to the moles of species \(i\) that were either reacted or produced. Finally, we used the molecular weight to convert moles to the desired mass of species \(i\).

A similar procedure can be used to calculate quantities such as the total moles reacted, the molar rate of reaction, or the molar flux due to reaction at the surface. The use of Faraday’s law and the more general procedure used to derive it are demonstrated in Illustration 1.3.

**ILLUSTRATION 1.3**

For a lead–acid battery, calculate the rate at which Pb reacts and \(\text{H}^+\) is consumed for a cell operating at 20 [A]. Express the rate of reaction in terms of a molar reaction rate.

The overall reaction for discharge is

\[
Pb + \text{PbO}_2 + 2\text{H}_2\text{SO}_4 \rightarrow 2\text{PbSO}_4 + 2\text{H}_2\text{O}
\]

The reaction at the positive electrode is

\[
Pb + \text{SO}_4^{2-} \rightarrow \text{PbSO}_4 + 2e^-, \quad \text{entry 17}
\]

The molar reaction rate of Pb (lead) consumption is obtained from Equation 1.11. \(Q\) is replaced with \(I\) to convert to a rate, and the molecular weight is not needed:

\[
\text{molar reaction rate of Pb} = \frac{I}{2F} = \frac{20}{2F} = 1.04 \times 10^{-4} \text{ mol s}^{-1}.
\]

The molar reaction rate of \(\text{H}^+\) is also obtained from Equation 1.11 in a similar fashion. However, the \(n\) value is different. In this case, we have 2 equivalents of charge (the 2 electrons in the half-cell reaction) for every 4 moles of \(\text{H}^+\). Therefore, \(n\) for \(\text{H}^+\) is 2/4 or 1/2 [equiv mol\(^{-1}\) \(\text{H}^+\)].

\[
\text{molar reaction rate of H}^+= \frac{I}{2F} = \frac{(2)20}{2F}
\]

\[
= 4.15 \times 10^{-4} \text{ mol s}^{-1}.
\]
Note that sulfate ions are produced at both electrodes. Based on the stoichiometry for the overall reaction, we expect 2 moles of sulfate ion to be consumed for each mole of Pb. Or, we can say that one mole of electrons react for each mole of sulfate. Formally, this is written as

\[
\text{molar reaction rate of } \text{SO}_4^{2-} = \frac{I}{nF} = \frac{20}{F} = 2.07 \times 10^{-4} \text{ mol s}^{-1}.
\]

Finally, we note that the reactants and products may be charged or neutral. They can also take several forms, such as a species dissolved in the electrolyte, a solid that deposits on the electrode, or a gas. Illustration 1.3 involved a solid reaction product, PbSO$_4$(s). Now let’s consider the oxidation of chloride ions in solution to form chlorine gas:

\[
2\text{Cl}^- \rightarrow \text{Cl}_2 + 2e^- \quad (1.12)
\]

Two chloride ions from solution each give up one electron and they combine at the metal surface to form the gas.

**ILLUSTRATION 1.4**

A current of 20 [A] passes for 10 minutes. How many grams of chlorine gas are produced assuming Equation 1.12 represents the electrode reaction? For ideal gas behavior, what volume of gas does this represent at atmospheric pressure (100 kPa) and at 25 °C?

Use Equation 1.11, \( n = 2, s_{\text{Cl}_2} = 1, M_{\text{Cl}_2} = 70.906 \text{ g mol}^{-1} \):

\[
m_i = \frac{M_iQ}{2F} = \frac{70.906(20)(10)(60)}{2(96485)} = 4.41 \text{ g.}
\]

The mass of \( \text{Cl}_2 \) is converted to moles (4.41/70.906), and the ideal gas law \( (pV = nRT) \) is used to determine the volume:

\[
\mathbf{V} = \left( \frac{m_i/M_i}{p} \right)RT = \frac{4.41/70.906\times(8.314)(298)}{100,000} = 0.0015 \text{ m}^3.
\]

**1.6 FARADAIC EFFICIENCY**

The electrochemical reactions that we have been discussing are called faradaic reactions since they involve electron transfer that is directly related to the consumption of reactants and the formation of products as described by Faraday’s law. To this point, we have only considered one reaction at each electrode. However, it is possible, and in fact common, for multiple reactions to take place at a single electrode in a real system. Frequently, one of the reactions is the desired reaction, and the other reactions are referred to as side reactions. In such cases, not all of the current goes into the desired reaction. We can define a faradaic efficiency to characterize the fraction of the total current that drives the desired reaction.

\[
\text{faradaic efficiency} = \frac{\text{amount of desired material produced}}{\text{amount that could be produced with the coulombs supplied}}
\]

Use of this efficiency is demonstrated in Illustration 1.5.

**ILLUSTRATION 1.5**

Nickel is electrodeposited from a bath of NiSO$_4$. A current of 1.0 A is passed for 3 hours and 3.15 g of Ni are deposited. What is the faradaic efficiency of this deposition?

The reaction is \( \text{Ni}^{2+} + 2e^- \rightarrow \text{Ni} \).

First, use Faraday’s law to determine how much Ni could possibly be deposited.

\[
m_i = \frac{M_iQ}{nF} = \frac{M_iIt}{nF} = \frac{58.7 \text{ [g mol}^{-1}] \times 1.0 \times [10 \text{[S]}^{-1}]] \times 3600 \text{[s/h]}]}{2 \text{[equiv/mol]} \times 96485 \text{[C/equiv]}} = 3.285 \text{ g Ni},
\]

\[
\eta_f = \frac{3.15}{3.285} = 0.96.
\]

One of the common side reactions for aqueous metal deposition is water hydrolysis to produce hydrogen gas.
1.7 CURRENT DENSITY

To this point in the chapter, we have considered the total current, \( I \). However, as you know from your experience, some electrochemical devices are small like a hearing aid battery. Others are significantly larger, such as the battery used to start your car. You would not expect the total current from these devices to be similar. Because electrochemical reactions take place on surfaces, we frequently normalize the total current by the surface area in order for us to better understand and characterize the system. **Current density** is defined as the current divided by the area of the electrode and will be used extensively throughout this book. Similarly, the molar rate of reaction is often expressed as a flux, \([\text{mol-m}^{-2}\cdot\text{s}^{-1}]\). These molar fluxes are used extensively in studying mass transfer. Let’s illustrate these concepts with an example.

### ILLUSTRATION 1.6

a. The electrode from Illustration 1.4 has an area of 80 cm\(^2\); what is the current density?

\[
i = \frac{I}{A} = \frac{20 \text{ [A]}}{0.008 \text{ [m}^2\text{]} } = 2500 \text{ [A-m}^{-2}\text{]}.\]

From Faraday’s law we can relate the charge to the amount of chloride ions that are consumed. Similar to current density, we define the flux of \( \text{Cl}^- \) to the electrode surface. Namely,

\[
N_{\text{Cl}^-} = \frac{i}{nF} = \frac{2500 \text{ [C/s – m}^2\text{]} }{(1\text{[equiv/mol]} \times 96485 \text{ [C/equiv]})} = 0.026 \text{ [mol-m}^{-2}\text{s}^{-1}].
\]

b. For the lead–acid battery described in Illustration 1.3, convert the molar reaction rates to molar fluxes given that the electrode area is 0.04 m\(^2\). The previous results are divided by the electrode area.

\[
\text{molar flux of Pb} = \frac{\text{rate of reaction}}{\text{electrode area}} = \frac{1.04 \times 10^{-4} \text{ [mol]} }{0.04} = 0.0026 \text{ mol m}^{-2}\text{s}^{-1}.
\]

This quantity represents the rate of dissolution of Pb from the negative electrode into the electrolyte.

Next, consider the flux of sulfate ion (see Illustration 1.3). Because sulfate is consumed at both electrodes, we must calculate the sulfate flux for each electrode.

### For the negative electrode,

\[
\text{molar flux of SO}_4^{2-} = \frac{I}{nF} = \frac{0.04}{2F} = 0.0026 \text{ mol m}^{-2}\text{s}^{-1}.
\]

### For the positive electrode,

\[
\text{molar flux of SO}_4^{2-} = \frac{I}{nF} = \frac{0.04}{2F} = 0.0026 \text{ mol m}^{-2}\text{s}^{-1}.
\]

Thus, we have 0.0026 mol m\(^{-2}\cdot\text{s}^{-1}\) of sulfate ions moving from the electrolyte toward the negative electrode and an equal flux moving toward the positive electrode.

Strictly speaking, molar flux, and therefore current density, are vector quantities—ones that have both a magnitude and direction. The current density, \( i \), is defined as

\[
i = \frac{I}{A} = F \sum z_i N_i, \quad (1.14)
\]

where \( N_i \) is the molar flux \([\text{mol-m}^{-2}\cdot\text{s}^{-1}]\) and \( z_i \) is the electrical charge of species \( i \). This equation indicates that for current to flow, there needs to be a net movement of charged species. We will only occasionally need to treat these quantities as having more than one directional component; therefore, our practice will be to not make any special effort to identify these quantities as vectors unless needed. However, even for one-dimensional current flow, we need to pay attention to the direction, which of course depends on how our coordinate system is defined. Referring back to Illustration 1.4, the flux of chloride ions is from right to left, which is a negative flux (in the negative \( x \) direction). The charge of the chloride ion, \( z_\text{Cl}^- \), is also negative. Therefore, current flow is positive in that example.

1.8 POTENTIAL AND OHM’S LAW

Another important quantity in the study of electrochemical systems is the potential. We can define an electrostatic potential, \( \phi \), in terms of the work required to move a unit (positive) charge from infinity to a specific position in the metal or in solution. This work can also be thought of in terms of energy. The unit for potential is a volt [V], which
is also [J⋅C\(^{-1}\)]. Since we are frequently interested in the potential of the electrodes, and since these are generally metals where electrons are the carriers of current, we can think of potential as a measure of the energy of the electron in the metal. Thus, the cell potential measured with a voltmeter in Figure 1.1 represents the difference in electron energy in the two electrodes.

As you may have guessed, the flow of current in metals and in electrolyte solutions is critical to the understanding and analysis of electrochemical systems. A potential difference in a metal or in an electrolyte leads to the flow of current. The difference is often expressed in terms of a potential gradient, which is the rate of change in potential with distance. By convention, electric current is defined as flowing from high potential to low potential, which is the direction that a positive charge would move due to the difference in the potential. This situation is illustrated in Figure 1.3. Current in a metal (e.g., wire) is due to electron flow. Since electrons are negatively charged, electrons travel from low potential to high potential. Ohm’s law relates the current and potential. For one-dimensional conduction (current flow),

\[ i_x = -\kappa \frac{d\phi}{dx}, \]  

(1.15)

where \( \kappa \) is the electrical conductivity of the electrolyte. The electrical conductivity is a property that characterizes how well the material moves electrical charge; it has units of [S⋅m\(^{-1}\)]. If the current density is constant, Equation 1.15 can be integrated to give

\[ \Delta\phi = \frac{iL}{\kappa}, \]  

(1.16)

This equation applies to one-dimensional current flow in an electrolyte of constant composition. A similar expression also applies to metals in general.

**ILLUSTRATION 1.7**

A fuel cell used for an automotive application operates at a current of 350 A. If the electrode area of each cell is 0.04 m\(^2\), what is the current density? If the distance between the electrodes is 0.07 mm, and the conductivity of the electrolyte is 10 S⋅m\(^{-1}\), what is the potential drop (difference in volts) across the electrolyte?

The current density, \( i \), is simply the current divided by the electrode area

\[ i = \frac{I}{A} = \frac{350}{0.04} = 8750 \text{ A} \cdot \text{m}^{-2}. \]

Ohm’s law is used to calculate the drop in potential across the electrolyte:

\[ \Delta\phi = \frac{iL}{\kappa} = \frac{8750(0.00007)}{10} = 0.06125 \text{ V} = 61 \text{ mV}. \]

Compare these results with the potential drop in 10 cm long copper wire with a diameter of 1 cm. The conductivity of copper is much higher: \( 5.85 \times 10^7 \text{ S} \cdot \text{m}^{-1} \). The same current flows through the wire, but the cross-sectional area \( (A_w = 7.9 \times 10^{-5} \text{ m}^{-2}) \) is smaller

\[ \Delta\phi = \frac{iL}{\kappa} = \frac{350}{\frac{58,500,000}{7.9 \times 10^{-5}(0.1)}} = 7.6 \text{ mV}. \]

**1.9 ELECTROCHEMICAL SYSTEMS: EXAMPLE**

We end this chapter with an example of an industrial electrolytic process—chlorine production by the chlor-alkali route. Our objectives in this section are twofold. First, to review principles and terminology within the context of an important electrochemical system. Second, to introduce the concept of the current–voltage relationship, also called the \( I-V \) curve. The connection between current and voltage is essential to any analysis of electrochemical systems. Finding and understanding this \( I-V \) relationship is a persistent theme of the book.

A simple representation of the electrochemical system for the chlor-alkali process is shown in Figure 1.4. The overall reaction can be written as

\[ 2\text{H}_2\text{O} + 2\text{Cl}^- \rightarrow \text{Cl}_2 + \text{H}_2 + 2\text{OH}^- \]  

(1.17)
In order to operate without interruption, reactants are supplied and products removed continuously. The reactant stream for the process is a purified brine of sodium chloride (NaCl), essentially a concentrated solution of salt water. The solution flows at a steady rate into the electrochemical cell, also called the electrochemical reactor. In addition to chlorine gas, sodium hydroxide and hydrogen are produced simultaneously in the process. Despite the appearance from the above equation, this reaction does not occur homogeneously. Instead, two heterogeneous electron-transfer reactions take place on separate metal surfaces:

$$2\text{Cl}^- \rightarrow \text{Cl}_2 + 2e^-$$
$$2\text{H}_2\text{O} + 2e^- \rightarrow \text{H}_2 + 2\text{OH}^-$$

The two metals on which the reactions occur are the electrodes, which are inert since they do not participate in the reactions. The electron-transfer reactions are faradaic processes and are governed by Faraday’s law. Oxidation takes place at the first electrode of our example, where two chloride ions lose electrons to form chlorine gas. Therefore, this electrode is the anode. The electrons enter the metal and travel through an external circuit. At the other electrode, the cathode, water is reduced to form hydrogen gas. The electrons consumed at the cathode are supplied by the external circuit, and the number of electrons produced at the anode is the same as the number consumed at the cathode. The electrolyte that is between the two electrodes contains ions of Na\(^+\), Cl\(^-\), and OH\(^-\). In this instance, there is a membrane separator that serves two functions: It keeps the two gaseous products apart and it allows sodium ions to move from the anode compartment to the cathode compartment, but excludes transport of anions. It is this movement of sodium ions that carries the current in the electrolyte. Note that there are three phases: solid (electrodes), liquid (electrolyte), and gas (reaction products). Furthermore, not all species are present in every phase. For instance, free electrons are found only in the metals, ions are confined to the electrolyte, and hydrogen gas is limited to the cathode. This heterogeneity is one of the defining characteristics of electrochemical systems—almost all of the action occurs at interfaces between the electrode and the electrolyte.

As you are probably beginning to appreciate, electrochemical systems are inherently complex. We’ve already seen that both electrodes are necessary and must be considered together. Many things happen at once: electron transfer, adsorption and desorption, transport of reactants and products, current flow in the electrolyte, and surface-mediated combination. In order to understand and analyze electrochemical systems, we’ll need to simultaneously apply our knowledge of thermodynamics, kinetics, and transport. These fundamental topics will be considered systematically in the chapters that follow.

Electrochemical cells are sometimes broken into two categories: galvanic and electrolytic. The two types have more similarities than differences, and are governed by the same engineering principles. The main distinction between them is that energy or electrical work is an output of a galvanic cell (e.g., a fuel cell or a battery discharging), whereas electrical energy is an input to electrolytic cells. We see in Figure 1.4 that a direct current (DC) power supply adds electrical work in the chlor-alkali process; therefore, this process is electrolytic.

An important feature of electrochemical systems is that current is an expression of the rate of reaction. In our example, the electrical current through the cell is directly related to the formation and consumption rates of hydrogen, chlorine, and sodium chloride through Faraday’s law. We can control the rate of reaction by controlling current. How much work is associated with this current flow? To answer this question, we need to know the potential of the cell. The potential is an expression of energy for charged species (electrons and ions), and provides the driving force needed for electrochemical reactions and for the flow of current in both metals and electrolytes.

We cannot simultaneously control the potential and current of an electrochemical system. If the potential applied to our electrolysis cell is increased, then the rate of hydrogen/chlorine production will also be increased. Alternatively, we might establish the rate of production by setting the current, but we would need to accept the resulting potential. These are the two basic modes of operation for electrochemical cells: potentiostatic (constant potential) or galvanostatic (constant current).

As mentioned above, a key objective in the analysis of any electrochemical system is to find the relationship between current and potential. The relationship can be