

FUEL CELL SYSTEMS EXPLAINED



ANDREW L. DICKS DAVID A. J. RAND



Fuel Cell Systems Explained

Fuel Cell Systems Explained

Third Edition

Andrew L. Dicks *Griffith University Brisbane, Australia*

David A. J. Rand *CSIRO Energy Melbourne, Australia*

WILEY

This edition first published 2018 © 2018 John Wiley & Sons Ltd

Edition History John Wiley & Sons Ltd (1e, 2000); John Wiley & Sons Ltd (2e, 2003)

All rights reserved. No part of this publication may be reproduced, stored in a retrieval system, or transmitted, in any form or by any means, electronic, mechanical, photocopying, recording or otherwise, except as permitted by law. Advice on how to obtain permission to reuse material from this title is available at http://www.wiley.com/go/permissions.

The right of Andrew L. Dicks and David A. J. Rand to be identified as the authors of this work has been asserted in accordance with law.

Registered Offices

John Wiley & Sons, Inc., 111 River Street, Hoboken, NJ 07030, USA John Wiley & Sons Ltd, The Atrium, Southern Gate, Chichester, West Sussex, PO19 8SQ, UK

Editorial Office

The Atrium, Southern Gate, Chichester, West Sussex, PO19 8SQ, UK

For details of our global editorial offices, customer services, and more information about Wiley products visit us at www.wiley.com.

Wiley also publishes its books in a variety of electronic formats and by print-on-demand. Some content that appears in standard print versions of this book may not be available in other formats.

Limit of Liability/Disclaimer of Warranty

While the publisher and authors have used their best efforts in preparing this work, they make no representations or warranties with respect to the accuracy or completeness of the contents of this work and specifically disclaim all warranties, including without limitation any implied warranties of merchantability or fitness for a particular purpose. No warranty may be created or extended by sales representatives, written sales materials or promotional statements for this work. The fact that an organization, website, or product is referred to in this work as a citation and/or potential source of further information does not mean that the publisher and authors endorse the information or services the organization, website, or product may provide or recommendations it may make. This work is sold with the understanding that the publisher is not engaged in rendering professional services. The advice and strategies contained herein may not be suitable for your situation. You should consult with a specialist where appropriate. Further, readers should be aware that websites listed in this work may have changed or disappeared between when this work was written and when it is read. Neither the publisher nor authors shall be liable for any loss of profit or any other commercial damages, including but not limited to special, incidental, consequential, or other damages.

Library of Congress Cataloging-in-Publication Data

Names: Dicks, Andrew L., author. | Rand, David A. J., 1942- author.

Title: Fuel cell systems explained / Andrew L. Dicks, Griffith University, Brisbane, Australia, David A. J. Rand, CSIRO Energy, Melbourne, Australia.

Description: Third edition. | Hoboken, NJ, USA : Wiley, [2018] | Includes bibliographical references and index. |

Identifiers: LCCN 2017054489 (print) | LCCN 2017058097 (ebook) | ISBN 9781118706978 (pdf) | ISBN 9781118706961 (epub) | ISBN 9781118613528 (cloth)

Subjects: LCSH: Fuel cells.

Classification: LCC TK2931 (ebook) | LCC TK2931 .L37 2017 (print) | DDC 621.31/2429–dc23 LC record available at https://lccn.loc.gov/2017054489

Cover design by Wiley

Cover images: Top Image: @ Iain Masterton/Alamy Stock Photo; Bottom Image: Courtesy of FuelCell Energy, Inc.

Set in 10/12pt Warnock by SPi Global, Pondicherry, India

Printed in the UK by Bell & Bain Ltd, Glasgow

 $10 \quad 9 \quad 8 \quad 7 \quad 6 \quad 5 \quad 4 \quad 3 \quad 2 \quad 1$

Contents

Brief Biographies xiii Preface xv Acknowledgments xvii Acronyms and Initialisms xix Symbols and Units xxv

- 1 Introducing Fuel Cells 1
- 1.1 Historical Perspective 1
- 1.2 Fuel-Cell Basics 7
- 1.3 Electrode Reaction Rates 9
- 1.4 Stack Design 11
- 1.5 Gas Supply and Cooling 14
- 1.6 Principal Technologies 17
- 1.7 Mechanically Rechargeable Batteries and Other Fuel Cells 19

v

- 1.7.1 Metal-Air Cells 20
- 1.7.2 Redox Flow Cells 20
- 1.7.3 Biological Fuel Cells 23
- 1.8 Balance-of-Plant Components 23
- 1.9 Fuel-Cell Systems: Key Parameters 24
- 1.10 Advantages and Applications 25 Further Reading 26

2 Efficiency and Open-Circuit Voltage 27

- 2.1 Open-Circuit Voltage: Hydrogen Fuel Cell 27
- 2.2 Open-Circuit Voltage: Other Fuel Cells and Batteries 31
- 2.3 Efficiency and Its Limits 32
- 2.4 Efficiency and Voltage 35
- 2.5 Influence of Pressure and Gas Concentration 36
- 2.5.1 Nernst Equation 36
- 2.5.2 Hydrogen Partial Pressure 38
- 2.5.3 Fuel and Oxidant Utilization 39
- 2.5.4 System Pressure 39
- 2.6 Summary 40 Further Reading 41

vi Contents

3 Operational Fuel-Cell Voltages 43

- 3.1 Fundamental Voltage: Current Behaviour 43
- 3.2 Terminology 44
- 3.3 Fuel-Cell Irreversibilities 46
- 3.4 Activation Losses 46
- 3.4.1 The Tafel Equation 46
- 3.4.2 The Constants in the Tafel Equation 48
- 3.4.3 Reducing the Activation Overpotential 51
- 3.5 Internal Currents and Fuel Crossover 52
- 3.6 Ohmic Losses 54
- 3.7 Mass-Transport Losses 55
- 3.8 Combining the Irreversibilities 57
- 3.9 The Electrical Double-Layer 58
- 3.10 Techniques for Distinguishing Irreversibilities 60
- 3.10.1 Cyclic Voltammetry 60
- 3.10.2 AC Impedance Spectroscopy 61
- 3.10.3 Current Interruption 65 Further Reading 68
- 4 Proton-Exchange Membrane Fuel Cells 69
- 4.1 Overview 69
- 4.2 Polymer Electrolyte: Principles of Operation 72
- 4.2.1 Perfluorinated Sulfonic Acid Membrane 72
- 4.2.2 Modified Perfluorinated Sulfonic Acid Membranes 76
- 4.2.3 Alternative Sulfonated and Non-Sulfonated Membranes 77
- 4.2.4 Acid–Base Complexes and Ionic Liquids 79
- 4.2.5 High-Temperature Proton Conductors 80
- 4.3 Electrodes and Electrode Structure 81
- 4.3.1 Catalyst Layers: Platinum-Based Catalysts 82
- 4.3.2 Catalyst Layers: Alternative Catalysts for Oxygen Reduction 85
- 4.3.2.1 Macrocyclics 86
- 4.3.2.2 Chalcogenides 87
- 4.3.2.3 Conductive Polymers 87
- 4.3.2.4 Nitrides 87
- 4.3.2.5 Functionalized Carbons 87
- 4.3.2.6 Heteropolyacids 88
- 4.3.3 Catalyst Layer: Negative Electrode 88
- 4.3.4 Catalyst Durability 88
- 4.3.5 Gas-Diffusion Layer 89
- 4.4 Water Management 92
- 4.4.1 Hydration and Water Movement 92
- 4.4.2 Air Flow and Water Evaporation 94
- 4.4.3 Air Humidity 96
- 4.4.4 Self-Humidified Cells 98
- 4.4.5 External Humidification: Principles 100
- 4.4.6 External Humidification: Methods *102*
- 4.5 Cooling and Air Supply 104

- 4.5.1 Cooling with Cathode Air Supply *104*
- 4.5.2 Separate Reactant and Cooling Air *104*
- 4.5.3 Water Cooling 105
- 4.6 Stack Construction Methods 107
- 4.6.1 Introduction 107
- 4.6.2 Carbon Bipolar Plates 107
- 4.6.3 Metal Bipolar Plates *109*
- 4.6.4 Flow-Field Patterns 110
- 4.6.5 Other Topologies 112
- 4.6.6 Mixed Reactant Cells 114
- 4.7 Operating Pressure 115
- 4.7.1 Technical Issues 115
- 4.7.2 Benefits of High Operating Pressures 117
- 4.7.2.1 Current 117
- 4.7.3 Other Factors 120
- 4.8 Fuel Types 120
- 4.8.1 Reformed Hydrocarbons 120
- 4.8.2 Alcohols and Other Liquid Fuels 121
- 4.9 Practical and Commercial Systems 122
- 4.9.1 Small-Scale Systems 122
- 4.9.2 Medium-Scale for Stationary Applications 123
- 4.9.3 Transport System Applications 125
- 4.10 System Design, Stack Lifetime and Related Issues 129
- 4.10.1 Membrane Degradation 129
- 4.10.2 Catalyst Degradation 129
- 4.10.3 System Control 129
- 4.11 Unitized Regenerative Fuel Cells *130* Further Reading *132*
- 5 Alkaline Fuel Cells 135
- 5.1 Principles of Operation 135
- 5.2 System Designs 137
- 5.2.1 Circulating Electrolyte Solution 137
- 5.2.2 Static Electrolyte Solution 140
- 5.2.3 Dissolved Fuel 142
- 5.2.4 Anion-Exchange Membrane Fuel Cells 144
- 5.3 Electrodes 147
- 5.3.1 Sintered Nickel Powder 147
- 5.3.2 Raney Metals 147
- 5.3.3 Rolled Carbon 148
- 5.3.4 Catalysts 150
- 5.4 Stack Designs 151
- 5.4.1 Monopolar and Bipolar 151
- 5.4.2 Other Stack Designs 152
- 5.5 Operating Pressure and Temperature 152
- 5.6 Opportunities and Challenges 155
 - Further Reading 156

viii Contents

6 Direct Liquid Fuel Cells 157

- 6.1 Direct Methanol Fuel Cells 157
- 6.1.1 Principles of Operation 160
- 6.1.2 Electrode Reactions with a Proton-Exchange Membrane Electrolyte 160
- 6.1.3 Electrode Reactions with an Alkaline Electrolyte 162
- 6.1.4 Anode Catalysts 162
- 6.1.5 Cathode Catalysts 163
- 6.1.6 System Designs 164
- 6.1.7 Fuel Crossover 165
- 6.1.8 Mitigating Fuel Crossover: Standard Techniques 166
- 6.1.9 Mitigating Fuel Crossover: Prospective Techniques 167
- 6.1.10 Methanol Production 168
- 6.1.11 Methanol Safety and Storage 168
- 6.2 Direct Ethanol Fuel Cells 169
- 6.2.1 Principles of Operation 170
- 6.2.2 Ethanol Oxidation, Catalyst and Reaction Mechanism 170
- 6.2.3 Low-Temperature Operation: Performance and Challenges 172
- 6.2.4 High-Temperature Direct Ethanol Fuel Cells 173
- 6.3 Direct Propanol Fuel Cells 173
- 6.4 Direct Ethylene Glycol Fuel Cells 174
- 6.4.1 Principles of Operation 174
- 6.4.2 Ethylene Glycol: Anodic Oxidation 175
- 6.4.3 Cell Performance 176
- 6.5 Formic Acid Fuel Cells 176
- 6.5.1 Formic Acid: Anodic Oxidation 177
- 6.5.2 Cell Performance 177
- 6.6 Borohydride Fuel Cells 178
- 6.6.1 Anode Catalysts 180
- 6.6.2 Challenges 180
- 6.7 Application of Direct Liquid Fuel Cells *182* Further Reading *184*

7 Phosphoric Acid Fuel Cells 187

- 7.1 High-Temperature Fuel-Cell Systems 187
- 7.2 System Design 188
- 7.2.1 Fuel Processing 188
- 7.2.2 Fuel Utilization 189
- 7.2.3 Heat-Exchangers 192
- 7.2.3.1 Designs 193
- 7.2.3.2 Exergy Analysis 193
- 7.2.3.3 Pinch Analysis 194
- 7.3 Principles of Operation 196
- 7.3.1 Electrolyte 196
- 7.3.2 Electrodes and Catalysts 198
- 7.3.3 Stack Construction 199
- 7.3.4 Stack Cooling and Manifolding 200
- 7.4 Performance 201

- 7.4.1 Operating Pressure 202
- 7.4.2 Operating Temperature 202
- 7.4.3 Effects of Fuel and Oxidant Composition 203
- 7.4.4 Effects of Carbon Monoxide and Sulfur 204
- 7.5 Technological Developments 204 Further Reading 206

8 Molten Carbonate Fuel Cells 207

- 8.1 Principles of Operation 207
- 8.2 Cell Components 210
- 8.2.1 Electrolyte 211
- 8.2.2 Anode 213
- 8.2.3 Cathode 214
- 8.2.4 Non-Porous Components 215
- 8.3 Stack Configuration and Sealing *215*
- 8.3.1 Manifolding 216
- 8.3.2 Internal and External Reforming 218
- 8.4 Performance 220
- 8.4.1 Influence of Pressure 220
- 8.4.2 Influence of Temperature 222
- 8.5 Practical Systems 223
- 8.5.1 Fuel Cell Energy (USA) 223
- 8.5.2 Fuel Cell Energy Solutions (Europe) 225
- 8.5.3 Facilities in Japan 228
- 8.5.4 Facilities in South Korea 228
- 8.6 Future Research and Development 229
- 8.7 Hydrogen Production and Carbon Dioxide Separation 230
- 8.8 Direct Carbon Fuel Cell 231 Further Reading 234

9 Solid Oxide Fuel Cells 235

- 9.1 Principles of Operation 235
- 9.1.1 High-Temperature (HT) Cells 235
- 9.1.2 Low-Temperature (IT) Cells 237
- 9.2 Components 238
- 9.2.1 Zirconia Electrolyte for HT-Cells 238
- 9.2.2 Electrolytes for IT-Cells 240
- 9.2.2.1 Ceria 240
- 9.2.2.2 Perovskites 241
- 9.2.2.3 Other Materials 243
- 9.2.3 Anodes 243
- 9.2.3.1 Nickel-YSZ 243
- 9.2.3.2 Cathode 245
- 9.2.3.3 Mixed Ionic-Electronic Conductor Anode 246
- 9.2.4 Cathode 247
- 9.2.5 Interconnect Material 247
- 9.2.6 Sealing Materials 248

x Contents

- 9.3 Practical Design and Stacking Arrangements 249
- 9.3.1 Tubular Design 249
- 9.3.2 Planar Design 251
- 9.4 Performance 253
- 9.5 Developmental and Commercial Systems 254
- 9.5.1 Tubular SOFCs 255
- 9.5.2 Planar SOFCs 256
- 9.6 Combined-Cycle and Other Systems 258 Further Reading 260
- **10** Fuels for Fuel Cells 263
- 10.1 Introduction 263
- 10.2 Fossil Fuels 266
- 10.2.1 Petroleum 266
- 10.2.2 Petroleum from Tar Sands, Oil Shales and Gas Hydrates 268
- 10.2.3 Coal and Coal Gases 268
- 10.2.4 Natural Gas and Coal-Bed Methane (Coal-Seam Gas) 270
- 10.3 Biofuels 272
- 10.4 Basics of Fuel Processing 275
- 10.4.1 Fuel-Cell Requirements 275
- 10.4.2 Desulfurization 275
- 10.4.3 Steam Reforming 277
- 10.4.4 Carbon Formation and Pre-Reforming 280
- 10.4.5 Internal Reforming 281
- 10.4.5.1 Indirect Internal Reforming (IIR) 283
- 10.4.5.2 Direct Internal Reforming (DIR) 283
- 10.4.6 Direct Hydrocarbon Oxidation 284
- 10.4.7 Partial Oxidation and Autothermal Reforming 285
- 10.4.8 Solar–Thermal Reforming 286
- 10.4.9 Sorbent-Enhanced Reforming 287
- 10.4.10 Hydrogen Generation by Pyrolysis or Thermal Cracking of Hydrocarbons 289
- 10.4.11 Further Fuel Processing: Removal of Carbon Monoxide 290
- 10.5 Membrane Developments for Gas Separation 293
- 10.5.1 Non-Porous Metal Membranes 293
- 10.5.2 Non-Porous Ceramic Membranes 294
- 10.5.3 Porous Membranes 294
- 10.5.4 Oxygen Separation 295
- 10.6 Practical Fuel Processing: Stationary Applications 295
- 10.6.1 Industrial Steam Reforming 295
- 10.6.2 Fuel-Cell Plants Operating with Steam Reforming of Natural Gas 296
- 10.6.3 Reformer and Partial Oxidation Designs 298
- 10.6.3.1 Conventional Packed-Bed Catalytic Reactors 298
- 10.6.3.2 Compact Reformers 299
- 10.6.3.3 Plate Reformers and Microchannel Reformers 300
- 10.6.3.4 Membrane Reactors 301
- 10.6.3.5 Non-Catalytic Partial Oxidation Reactors 302

Contents xi

- 10.6.3.6 Catalytic Partial Oxidation Reactors 303
- 10.7 Practical Fuel Processing: Mobile Applications 304
- 10.8 Electrolysers 305
- 10.8.1 Operation of Electrolysers 305
- 10.8.2 Applications 307
- 10.8.3 Electrolyser Efficiency *312*
- 10.8.4 Photoelectrochemical Cells 312
- 10.9 Thermochemical Hydrogen Production and Chemical Looping 314
- 10.9.1 Thermochemical Cycles 314
- 10.9.2 Chemical Looping 317
- 10.10 Biological Production of Hydrogen 318
- 10.10.1 Introduction 318
- 10.10.2 Photosynthesis and Water Splitting 318
- 10.10.3 Biological Shift Reaction 320
- 10.10.4 Digestion Processes 320 Further Reading 321
- 11 Hydrogen Storage 323
- 11.1 Strategic Considerations 323
- 11.2 Safety 326
- 11.3 Compressed Hydrogen 327
- 11.3.1 Storage Cylinders 327
- 11.3.2 Storage Efficiency 329
- 11.3.3 Costs of Stored Hydrogen 330
- 11.3.4 Safety Aspects 330
- 11.4 Liquid Hydrogen 331
- 11.5 Reversible Metal Hydrides 333
- 11.6 Simple Hydrogen-Bearing Chemicals 338
- 11.6.1 Organic Chemicals 338
- 11.6.2 Alkali Metal Hydrides 339
- 11.6.3 Ammonia, Amines and Ammonia Borane 340
- 11.7 Complex Chemical Hydrides 341
- 11.7.1 Alanates 342
- 11.7.2 Borohydrides 342
- 11.8 Nanostructured Materials 344
- 11.9 Evaluation of Hydrogen Storage Methods 347 Further Reading 350
- **12** The Complete System and Its Future *351*
- 12.1 Mechanical Balance-of-Plant Components 351
- 12.1.1 Compressors 351
- 12.1.1.1 Efficiency 354
- 12.1.1.2 Power 356
- 12.1.1.3 Performance Charts 356
- 12.1.1.4 Selection 359
- 12.1.2 Turbines 361
- 12.1.3 Ejector Circulators 362

- xii Contents
 - 12.1.4 Fans and Blowers 363
 - 12.1.5 Pumps 364
 - 12.2 Power Electronics 365
 - 12.2.1 DC Regulators (Converters) and Electronic Switches 366
 - 12.2.2 Step-Down Regulators 368
 - 12.2.3 Step-Up Regulators 370
 - 12.2.4 Inverters 371
 - 12.2.4.1 Single Phase 372
 - 12.2.4.2 Three Phase 376
 - 12.2.5 Fuel-Cell Interface and Grid Connection Issues 378
 - 12.2.6 Power Factor and Power Factor Correction 378
 - 12.3 Hybrid Fuel-Cell + Battery Systems 380
 - 12.4 Analysis of Fuel-Cell Systems 384
 - 12.4.1 Well-to-Wheels Analysis 385
 - 12.4.2 Power-Train Analysis 387
 - 12.4.3 Life-Cycle Assessment 388
 - 12.4.4 Process Modelling 389
 - 12.4.5 Further Modelling 392
 - 12.5 Commercial Reality 394
 - 12.5.1 Back to Basics 394
 - 12.5.2 Commercial Progress 395
 - 12.6 Future Prospects: The Crystal Ball Remains Cloudy 397 Further Reading 399

Appendix 1 Calculations of the Change in Molar Gibbs Free Energy 401

- A1.1 Hydrogen Fuel Cell 401
- A1.2 Carbon Monoxide Fuel Cell 403

Appendix 2 Useful Fuel-Cell Equations 405

- A2.1 Introduction 405
- A2.2 Oxygen and Air Usage 406
- A2.3 Exit Air Flow Rate 407
- A2.4 Hydrogen Usage 407
- A2.5 Rate of Water Production 408
- A2.6 Heat Production 409

Appendix 3 Calculation of Power Required by Air Compressor and Power Recoverable by Turbine in Fuel-Cell Exhaust 411

- A3.1 Power Required by Air Compressor 411
- A3.2 Power Recoverable from Fuel-Cell Exhaust with a Turbine 412

Glossary of Terms 415 Index 437

Brief Biographies



Andrew L. Dicks

Andrew L. Dicks, PhD, CChem, FRSC, was educated in England and graduated from Loughborough University before starting a career in the corporate laboratories of the UK gas industry. His first research projects focused on heterogeneous catalysts in gas-making processes, for which he was awarded a doctorate in 1981. In the mid-1980s, BG appointed Andrew to lead a research effort on fuel cells that was directed predominantly towards molten carbonate and solid oxide systems. The team pioneered the application of process modelling to fuel-cell systems, especially those that featured internal reforming. This work, which was supported by the European Commission during the 1990s, involved collaboration with leading fuel-cell developers throughout Europe and North America. In 1994, Andrew was jointly awarded the Sir Henry Jones

(London) Medal of the Institution of Gas Engineers and Managers for his studies on high-temperature systems. He also took an interest in proton-exchange membrane fuel cells and became the chair of a project at the University of Victoria, British Columbia, in which Ballard Power Systems was the industrial partner. In 2001, he was awarded a Senior Research Fellowship at the University of Queensland, Australia, that enabled further pursuit of his interest in catalysis and the application of nanomaterials in fuelcell systems. Since moving to Australia, he has continued to promote hydrogen and fuel-cell technology, as director of the CSIRO National Hydrogen Materials Alliance and as a director of the Australian Institute of Energy. He is now consulted on energy and clean technology issues by governments and funding agencies worldwide.



David A. J. Rand

David A. J. Rand, AM, BA, MA, PhD, ScD, FTSE, was educated at the University of Cambridge where, after graduation, he conducted research on lowtemperature fuel cells. In 1969, he joined the Australian government's CSIRO laboratories in Melbourne. After further exploration of fuel-cell mechanisms and then electrochemical studies of mineral beneficiation, he formed the CSIRO Novel Battery Technologies Group in the late 1970s and

remained its leader until 2003. He was one of the six scientists who established the USbased Advanced Lead–Acid Battery Consortium in 1992 and served as its manager in 1994. He is the co-inventor of the UltraBatteryTM, which finds service in hybrid electric vehicle and renewable energy storage applications. As a chief research scientist, he fulfilled the role of CSIRO's scientific advisor on hydrogen and renewable energy until his retirement in 2008. He remains active within the organisation as an Honorary Research Fellow and has served as the chief energy scientist of the World Solar Challenge since its inception in 1987. He was awarded the Faraday Medal by the Royal Society of Chemistry (United Kingdom) in 1991, the UNESCO Gaston Planté Medal by the Bulgarian Academy of Sciences in 1996 and the R.H. Stokes Medal by the Royal Australian Chemical Institute in 2006. He was elected a fellow of the Australian Academy of Technological Sciences and Engineering in 1998 and became a member of the Order of Australia in 2013 for service to science and technological development in the field of energy storage.

Preface

Since publication of the first edition of *Fuel Cell Systems Explained*, three compelling drivers have supported the continuing development of fuel-cell technology, namely:

- The need to maintain energy security in an energy-hungry world.
- The desire to reduce urban air pollution from vehicles.
- The mitigation of climate change by lowering anthropogenic emissions of carbon dioxide.

New materials for fuel cells, together with improvements in the performance and lifetimes of stacks, are underpinning the emergence of the first truly commercial systems in applications that range from forklift trucks to power sources for mobile phone towers. Leading vehicle manufacturers have embraced the use of electric drivetrains and now see hydrogen fuel cells complementing the new battery technologies that have also emerged over the past few years. After many decades of laboratory development, a global — but fragile — fuel-cell industry is bringing the first products to market.

To assist those who are unfamiliar with fuel-cell electrochemistry, Chapter 1 of this third edition has been expanded to include a more detailed account of the evolution of the fuel cell and its accompanying terminology. In the following chapters, extensive revision of the preceding publication has removed material that is no longer relevant to the understanding of modern fuel-cell systems and has also introduced the latest research findings and technological advances. For example, there are now sections devoted to fuel-cell characterization, new materials for low-temperature hydrogen and liquid-fuelled systems, and a review of system commercialization. Separate chapters on fuel processing and hydrogen storage have been introduced to emphasize how hydrogen may gain importance both in future transport systems and in providing the means for storing renewable energy.

The objective of each chapter is to encourage the reader to explore the subject in more depth. For this reason, references have been included as footnotes when it is necessary to substantiate or reinforce the text. To stimulate further interest, however, some recommended further reading may be given at the end of a chapter.

There are now several books and electronic resources available to engineers and scientists new to fuel-cell systems. The third edition of *Fuel Cell Systems Explained* does not intend to compete with specialist texts that can easily be accessed via the Internet. Rather, it is expected that the book will continue to provide an introduction and overview for students and teachers at universities and technical schools and act as

xvi Preface

a primer for postgraduate researchers who have chosen to enter this field of technology. Indeed, it is hoped that *all* readers — be they practitioners, researchers and students in electrical, power, chemical and automotive engineering disciplines — will continue to benefit from this essential guide to the principles, design and implementation of fuel-cell systems.

December 2017

Andrew L. Dicks, Brisbane, Australia David A. J. Rand, Melbourne, Australia

Acknowledgments

As emphasized throughout this publication, the research and development of fuel cells is highly interdisciplinary in that it encompasses many aspects of science and engineering. This fact is reflected in the number and diversity of companies and organizations that have willingly provided advice and information or given permission to use their images in the third edition of *Fuel Cell Systems Explained*. Accordingly, the authors are indebted to the following contributors:

Avantica plc (formerly BG Technology Ltd), UK Ballard Power Systems Inc., USA CNR ITAE, Italy Coregas, Australia Cygnus Atratus, UK Daimler AG, Germany Doosan Fuel Cell, USA Eaton Corporation, USA Forschungszentrum Jülich GmbH, Germany Fuel Cell Energy, USA Horizon Fuel Cells, Singapore Hydrogenics Corporation, Canada Hyundai Motor Company, Australia Pty Ltd Intelligent Energy, UK International Fuel Cells, USA ITM Power, UK Johnsons Matthey plc, UK Kawasaki Heavy Industries, Japan Kyocera, Japan NDC Power, USA Osaka Gas, Japan Proton Energy Systems, USA Proton Motor Systems, GmbH, Germany Redflow Ltd, Australia Serenergy, Denmark Siemens Westinghouse Power Corporation, USA

In addition, the authors acknowledge the work of James Larminie, who instigated the first edition of this book, as well as the assistance of others engaged in the advancement

xviii Acknowledgments

of fuel cells, namely, John Appleby (Texas A&M University, USA), Nigel Brandon and David Hart (Imperial College, UK), John Andrews (RMIT University, Australia), Evan Gray (Griffith University, Australia), Ian Gregg (Consultant, Australia) and Chris Hodrien (University of Warwick, UK).

The authors also wish to express their thanks for the support and encouragement given by family, friends and colleagues during the course of this project.

Acronyms and Initialisms

ABPBI	phosphoric acid doped poly(2,5-benzimidazole)
AC	alternating current
ADP	adenosine 5'-triphosphate
AEM	alkaline-electrolyte membrane
AEMFC	alkaline-electrolyte membrane fuel cell
AES	air-electrode supported
AFC	alkaline fuel cell
AMFC	anion-exchange membrane fuel cell
ANL	Argonne National Laboratory
APEMFC	alkaline proton-exchange membrane fuel cell
APU	auxiliary power unit
ASR	area specific resistance
BCN	Dutch Fuel Cell Corporation
BG	British Gas
BIMEVOX	bismuth metal vanadium oxide $(Bi_4V_2O_{11})$
BOP	balance-of-plant
BPS	Ballard Power Systems
BSF	Boudouard Safety Factor
CAN bus	Controller Area Network
CBM	coal-bed methane
CCS	carbon capture and storage
CFCL	Ceramic Fuel Cells Ltd
CGO	cerium–gadolinium oxide (same as GDC)
CHP	combined heat and power
CLC	chemical looping combustion
CNR	Consiglio Nazionale delle Ricerche (Italy)
CNT	carbon nanotube
CODH-1	carbon monoxide dehydrogenase
CPE	constant phase element
CPO	catalytic partial oxidation
CRG	catalytic rich gas
CSG	coal-seam gas
CSIRO	Commonwealth Scientific and Industrial Research Organisation

xix

xx Acronyms and Initialisms

CSO	cerium-samarium oxide (same as SDC)
CSZ	calcia-stabilized zirconia
CV	cyclic voltammetry
CVD	chemical vapour deposition
DBFC	direct borohydride fuel cell
DC	direct current
DCFC	direct carbon fuel cell
DEFC	direct ethanol fuel cell
DEGEC	direct ethylene glycol fuel cell
DFAFC	direct formic acid fuel cell (also formic acid fuel cell FAFC)
DFT	density functional theory
DG	distributed generator
	direct internal referming
	directly implicated values at a solution reactor
	directly irradiated, volumetric receiver-reactor
DLFC	
DMFC	direct methanol fuel cell
DOE	Department of Energy (United States)
DPFC	direct propanol fuel cell
DPFC(2)	direct propan-2-ol fuel cell
DSSC	dye-sensitized solar cell
EC	evaporatively cooled
ECN	Energy Research Centre of the Netherlands
EFOY	Energy for You
EIS	electrochemical impedance spectroscopy
EPFL	Swiss Federal Institute of Technology
EU	European Union
EVD	electrochemical vapour deposition
EW	membrane equivalent weight
FCE	Fuel Cell Energy Inc.
FCES	Fuel Cell Energy Solutions GmbH
FCV	fuel cell vehicle
FRA	frequency response analyser
FT	Fischer–Tropsch
	L
GDC	gadolinium-doped ceria/gadolinia-doped ceria (same as CGO)
GDL	gas-diffusion laver
GE	General Electric
GHG	greenhouse gas
GM	General Motors
GPS	Global Positioning System
GTI	gas-to-liquid
GTO	gate turn-off (thyristor)
010	gaie (1111-011 (111115101)
	hazard identification
	hazard and anovability study
TIALOP	nazaru anu operability study

HCNG	hydrogen-compressed natural gas
HDS	hydrodesulfurization
HEMFC	hydroxide-exchange polymer membrane fuel cell
HEV	hybrid electric vehicle
HHV	higher heating value
HOR	hydrogen oxidation reaction
HPE	high-pressure proton-exchange membrane electrolyser
IREC	indirect borobydride fuel cell
ICE	internal combustion angine
ICEV	internal combustion engine vahiale
	International Eval Colla
	Insulated-gate Dipolar transistor
	isnikawajima-Harima Heavy Industries Co., Ltd
	indirect internal reforming (also known as integrated reforming)
IIM IT COFC	ion transport membrane, also refers to company ITM Power
IT-SOFC	intermediate-temperature solid oxide fuel cell
IUPAC	International Union of Pure and Applied Chemistry
KEPCO	Korea Electric Power Corporation
KIST	Korea Institute of Science and Technology
LAMOX	lanthanum molybdate (La2M02O9)
LCA	life-cycle assessment (also known as 'life-cycle analysis' and 'cradle-to-grave
	analysis')
LCOE	levelized cost of electricity
LH_2	liquid hydrogen
LHV	lower heating value
LNG	liquefied natural gas
LPG	liquefied petroleum gas
LSCF	lanthanum strontium cobaltite ferrite
LSCV	strontium-doped lanthanum vanadate
LSGM	lanthanum gallate (LaSrGaMgO ₃)
LSM	strontium-doped lanthanum manganite
LT-SOFC	low-temperature solid oxide fuel cell
MCFC	molten carbonate fuel cell
MCR	microchannel reactor
MEA	membrane_electrode assembly
MEMS	microelectromechanical systems
METI	Ministry of Economy Trade and Industry (Japan)
MFC	microbial fuel cell
MFF	mass flow factor
MHPS	Mitsuhishi Hitachi Power Systems
MIEC	mixed ionic_electronic conductor (ovides)
MOE	matal organic framework
MOSEET	metal oxido somiconductor field offect transistor
MOSFEI	metal-oxide-semiconductor neid-enect transistor

xxii Acronyms and Initialisms

MPMDMS	(3-mercaptopropyl)methyldimethoxysilane		
MRFC	mixed-reactant fuel cell		
MSW	municipal solid waste		
MTBF	mean time between failures		
MWCNT	multiwalled carbon nanotube		
NADP	nicotinamide adenine dinucleotide phosphate		
NASA	National Aeronautics and Space Administration		
NCPO	non-catalytic partial oxidation		
NEDO	New Energy Development Organization (Japan)		
NOMO	Notice of Market Opportunities		
NTP	normal temperature and pressure		
OCV	open-circuit voltage		
OEM	original equipment manufacturer		
OER	oxygen evolution reaction		
OHP	outer Helmholtz plane		
ORR	oxygen reduction reaction		
P2G	power-to-gas		
P3MT	poly(3-methylthiophene)		
PAFC	phosphoric acid fuel cell		
PANI	polyaniline		
PAR	photosynthetically active radiation		
PBI	polybenzimidazole		
PBSS	poly(benzylsulfonic acid)siloxane		
PC	phthalocyanine		
PCT	pressure composition isotherm		
PEC	photoelectrochemical cell		
PEMFC	proton-exchange membrane fuel cell (also called 'polymer electrolyte		
	membrane fuel cell' and same as SPEFC and SPFC)		
PET	polyethylene terephthalate		
PF	power factor, also PFC power factor correction		
PFD	process flow diagram		
PFSA	perfluorinated sulfonic acid		
plc	programmable logic controller		
POX	partial oxidation		
PPA	polyphosphoric acid		
PPBP	poly(1,4-phenylene), poly(4 phenoxybenzoyl-1,4-phenylene)		
Рру	polypyrrole		
PROX	preferential oxidation		
PrOx	preferential oxidation reactor		
PSA	pressure swing adsorption		
PTFE	polytetrafluoroethylene		
PV	photovoltaic		
PWM	pulse width modulation		
QA	quaternary ammonium		

RDE	rotating disc electrode
RFB	redox flow battery
RH	relative humidity
RHE	reversible hydrogen electrode
RRDE	rotating ring-disc electrode
RSF	rotational speed factor
	-
SATP	standard ambient temperature and pressure
SCG	simulated coal gas
SCT-CPO	short contact time catalytic partial oxidation
SDC	samarium-doped ceria/samaria-doped ceria (same as CSO)
SECA	Solid State Energy Conversion Alliance
SFCM	standard cubic foot per minute
SHE	standard hydrogen electrode
SI	International System of Units (French: Système international d'unités)
SLM	standard litre per minute
SMR	steam reforming reaction
SNG	substitute natural gas (also synthetic natural gas)
SOFC	solid oxide fuel cell
m-SPAEEN-60	sulfonated poly(arylene ether ether nitrile)
SPEEK	sulfonated polyether ether ketone
SPEFC	solid polymer electrolyte fuel cell (same as PEMFC)
SPFC	solid polymer fuel cell (same as PEMFC)
SPOF	single point of failure
STP	standard temperature and pressure
SWPC	Siemens Westinghouse Power Corporation
TAA	tetraazaannulene
THT	tetrahydrothiophene
TMPP	tetramethoxyphenylporphyrin
TPP	tetraphenylporphyrin
TPTZ	2, 4, 6-tris(2-pyridyl)-1,3,5-triazine
TTW	tank-to-wheel
UCC	Union Carbide Corporation
UK	United Kingdom
ULP	unleaded petrol
UPS	uninterruptible power system; also uninterruptible power supply
URFC	unitized regenerative fuel cell
USA	United States of America
USB	universal serial bus
UTC	United Technologies Corporation
UV	ultraviolet
WGS	water_gas shift
WTT	wall-to_tonk
WTW	well-to-uheele
VV I VV	
XPS	X-ray photoelectron spectroscopy

Symbols and Units

Subunits			Multiple units		
d	deci	10^{-1}	k	kilo	10 ³
С	centi	10^{-2}	М	mega	10^{6}
m	milli	10^{-3}	G	giga	10^{9}
μ	micro	10^{-6}	Т	tera	10^{12}
n	nano	10^{-9}	Р	peta	10^{15}

- A ampere
- A electrode area (cm^2), also coefficient in natural logarithm form of the Tafel equation
- Ah ampere hour
- *a* chemical activity; also coefficient in base 10 logarithm form of the Tafel equation
- a_x chemical activity of species x
- atm atmosphere (=101.325 kPa)
- *B* exergy (J)
- ΔB change in exergy (J)
- bbl barrel of oil: 35 imperial gallons (159.113 L), or 42 US gallons (158.987 L)
- bar unit of pressure (=100 kPa)
- bhp brake horsepower (=745.7 W)
- C constant in various equations; also coulomb (=1A s), the unit of electric charge
- °C degree Celsius
- C_P specific heat capacity at constant pressure (J kg⁻¹ K⁻¹)
- C_V specific heat capacity at constant volume (J kg⁻¹K⁻¹)
- $\overline{c_P}$ molar heat capacity at constant pressure ($J \mod^{-1} K^{-1}$)
- $\overline{c_V}$ molar heat capacity at constant volume (J mol⁻¹ K⁻¹)
- cm centimetre
- D_m diffusion coefficient (m² s⁻¹)
- d separation of charge layers in a capacitor (mm)
- *E* electrode potential (V)
- E° standard electrode potential (V)
- E_r reversible electrode potential (V)
- E_r° standard reversible electrode potential (V)

xxvi Symbols and Units

EW	(membrane) equivalent weight
e^-	electron, or the charge on one electron $(=1.602 \times 10^{-19} \text{ coulombs})$
ΔE_{act}	activation overpotential (V)
F	farad, unit of electrical capacitance $(s^4 A^2 m^{-2} kg^{-1})$
F	Faraday constant (=96 458 coulombs mol^{-1})
ft	foot (linear measurement = $305 \mathrm{mm}$)
G	Gibbs free energy (I)
ΛG	change in Gibbs free energy (I)
ΔG°	change in standard Gibbs free energy (I)
G°	standard Cibbs free energy of formation (I)
ΔC°	shanga in standard Cibbs free energy of formation (I)
$\overline{\alpha}$	moles Cibbs free energy (Ime l^{-1})
g A=	$\frac{1}{1000} = \frac{1}{1000} = 1$
Δg	change in molar Gibbs free energy () mol)
Δg°	change in standard molar Gibbs free energy () mol ^{-1})
Δg_f	change in molar Gibbs free energy of formation () mol ⁻¹)
$\Delta \overline{g}_{f}^{\circ}$	change in standard molar Gibbs free energy of formation (J mol ⁻¹)
g	gram
g	acceleration due to gravity (m s^{-2})
Η	enthalpy (J)
ΔH	change in enthalpy (J)
ΔH°	change in standard enthalpy (J)
H_f°	standard enthalpy of formation (J)
ΔH_f°	change in standard enthalpy (heat) of formation (J)
\overline{h}	molar enthalpy (J mol ⁻¹)
$\Delta \overline{h}$	change in molar enthalpy (Jmol ⁻¹)
$\Delta \overline{h}^{\circ}$	change in standard molar enthalpy (Jmol ⁻¹)
$\Delta \overline{h}_f$	change molar enthalpy of formation $(J mol^{-1})$
$\Delta \overline{h}_{f}^{\circ}$	change in standard molar enthalpy of formation $(J mol^{-1})$
h	hour
IR_{e}^{\prime}	resistive loss in electrolyte (Ω)
$IR_{t}^{\tilde{I}}$	total resistive loss in electrodes (Ω)
I	current (A)
i	current density, i.e., current per unit area (usually expressed in mA cm ^{-2})
i.	crossover current (A)
i,	limiting current density (usually expressed in mA cm ^{-2})
i.	exchange-current density (usually expressed in mA cm^{-2})
ι Γ	ioule (-1 W/s)
) K	kelvin (used as a measure of absolute temperature)
I	litro
MEE	mass flow factor $(kgs^{-1}K^{1/2}bar^{-1})$
m	matra
111	metre mass flow rate e.g. of gas $(\log s^{-1})$ or of a liquid $(mlmin^{-1})$
111	mass flow rate, e.g., or gas (kgs) of or a liquid (infinition) mass of substance $r(g)$
m_x	millioguivalant (weight) (mg I ⁻¹)
mel	milliequivalent (weight) (ing L_{j}
mol	more, i.e., mass or $6.022 \times 10^{\circ}$ elementary units (atoms, molecules, etc.)
NI	substance $(unit of force - 1) com e^{-2}$
IN	newton (unit of force = 1 kg m s)

of a

Ν	rotor speed of fan (revolutions per minute)
N_{Λ}	Avogadro's number, $6.022140857 \times 10^{23}$
N-m ³	normal cubic metre of gas (i.e., that measured at NTP)
n	number of units (electrons, atoms, molecules) involved in a chemical or elec-
	trochemical reaction: also number of cells in fuel-cell stack
n.	number of units or moles of species <i>i</i>
n 'n	molar flow rate of species r (mols ⁻¹)
P	pressure (in Pa or bar)
P	power (W) only used when context is clear that pressure is not under discussion
P°	standard pressure (-100 kPa)
Perm	saturated vapour pressure
P	partial pressure of species r
$\mathbf{P}_{\mathbf{x}}$	parcal (1 Pa = 1 N m ⁻² - 9.869 × 10^{-6} atm)
nnh	parts per billion
рН	numerical scale used to specify the acidity or basicity of an aqueous solution
ppm	parts per million
PP ^{III} R	$gas constant (-8.1345 I K^{-1} mol^{-1})$
$R^{/}$	resistance (Ω)
R	internal resistance of a transistor
RH	relative humidity (%): also denoted by the symbol $\phi(vi)$
®	registered trademark/convright
r	area specific resistance ($\Omega \text{ cm}^2$)
S	siemens unit of conductance (Ω^{-1})
S	entropy (IK^{-1})
<u>AS</u>	change in entropy (JK^{-1})
ΔS°	change in standard entropy (IK^{-1})
$S^{\circ}_{\mathcal{L}}$	standard entropy of formation (IK^{-1})
ΔS°_{f}	change in standard entropy of formation (JK^{-1})
\overline{s}	molar entropy $(IK^{-1}mol^{-1})$
$\Delta \overline{s}$	change in molar entropy $(JK^{-1}mol^{-1})$
$\Delta \overline{s}^{\circ}$	change in standard molar entropy (Imol^{-1})
$\Delta \overline{s}_{f}$	change in molar entropy of formation $(Imol^{-1})$
$\Delta \overline{s}_{f}^{\circ}$	change in standard molar entropy of formation $(Imol^{-1})$
s	second
SLM	standard litre per minute
Т	temperature
ТМ	trademark
t	tonne
$t_{1/2}$	half-life
V	volt
V_c	cell voltage (V)
V_r	reversible cell voltage; also known as 'open-circuit voltage' (V)
V_r°	reversible cell voltage (V) under standard conditions of temperature (298.15 K)
	and pressure (101.325 kPa)
ΔV_{gain}	voltage gain (V)
ΔV_{loss}	voltage loss (V)
vol.%	volume percent

xxviii Symbols and Units

- *W* work done, e.g., in compressing a gas (J)
- *W*′′ isentropic work (J)
- W watt
- W_{el} watt, electrical power
- W_{th} watt, thermal power
- Wh watt-hour
- wt.% weight percent
- x_i mole fraction of species i in solution
- Z impedance (Ω)
- *z* number of units (electrons, atoms, molecules) involved in a chemical or electrochemical reaction
- α charge transfer coefficient
- γ ratio of the specific heats of a gas $C_P: C_V$
- δ_m thickness of proton exchange membrane (cm)
- ε electrical permittivity (F m⁻¹)
- ξ electro-osmotic coefficient
- η electrode overpotential (V); also efficiency (%) (e.g., of a fuel cell)
- η_+ overpotential at a positive electrode (V)
- η_{-} overpotential at a negative electrode (V)
- η_C is entropic compressor efficiency (%)
- η_f fuel utilization coefficient (%), a 'figure of merit' for DMFCs
- $\hat{\vartheta}$ phase angle
- λ stoichiometric ratio
- μ_f fuel utilization coefficient
- μ_i chemical potential of species *i* (J kg⁻¹ or J mol⁻¹)
- μ gas viscosity (centipoise, cP = 0.001 kg m⁻¹ s⁻¹)
- ϕ relative humidity (usually expressed as a percentage); also denoted by RH
- ρ gas density (kg m⁻³)
- ω humidity ratio, also known as 'absolute humidity' and 'specific humidity'; symbol also used for radial frequency
- Ω ohm